

Air Receiver using Prode Physical Properties

Modified from a worksheet by Oscar Delgado to demonstrate the use of Prode Physical Properties (PPP) within Mathcad.

```
mc_AOpen("") = 0          opened test2.hpp archive  
stream := 20  
mc_edS(20) = 1          create stream 20 in Prode window for dry air  
SRK standard model
```

Input

$\phi_{hum} := 0.1$		
pressure bands, Pa abs	temperatures, avg	process requirements
Pressure1 := (135 + 14.7)·psi	Temp := 129 °F	time := 30·min
Pressure2 := (50 + 14.7)·psi	Temp _{atm} := 77 °F	flow _{req} := 32· $\frac{\text{ft}^3}{\text{min}}$
P _{atm} := 14.7·psi		

Saturation pressure from Prode Physical Properties

H₂O_code := mc_getCC(stream, 3) = 1.631×10^3 component # for water in PPP database

$$P_{sat_temp} := mc_CompVP\left(H_2O_code, \frac{Temp}{K}\right) \cdot Pa = 2.168 \cdot psi$$
$$P_{sat_temp_atm} := mc_CompVP\left(H_2O_code, \frac{Temp_{atm}}{K}\right) \cdot Pa = 0.461 \cdot psi$$

Computations

$$P_{H2O_temp} := \phi_{hum} \cdot P_{sat_temp} = 0.217 \cdot psi$$

$$P_{H2O_temp_atm} := \phi_{hum} \cdot P_{sat_temp_atm} = 0.046 \cdot psi$$

compositions

$$y_{H2O_P1} := \frac{P_{H2O_temp}}{\text{Pressure1}} = 1.449 \times 10^{-3}$$

$$y_{H2O_P2} := \frac{P_{H2O_temp}}{\text{Pressure2}} = 3.351 \times 10^{-3}$$

$$y_{H2O_avg} := \frac{y_{H2O_P1} + y_{H2O_P2}}{2} \quad y_{air} := 1 - y_{H2O_avg} = 0.998$$

$$y_{H2O_atm} := \frac{P_{H2O_temp_atm}}{P_{atm}} = 3.139 \times 10^{-3} \quad y_{air_atm} := 1 - y_{H2O_atm} = 0.997$$

$$\text{comp} := \begin{pmatrix} .79 \\ .21 \end{pmatrix} \cdot y_{air} \quad \text{comp}_{atm} := \begin{pmatrix} .79 \\ .21 \end{pmatrix} \cdot y_{air_atm}$$

$$\text{comp} := \text{stack}(\text{comp}, y_{H2O_avg}) \quad \text{comp}_{atm} := \text{stack}(\text{comp}_{atm}, y_{H2O_atm})$$

modify stream 20 composition in Prode archive and obtain density

```
GD(str,x,t,p) := | n ← rows(x)
                  "change the composition"
                  for i ∈ 0 .. n - 1
                      valid_xi ← mc_putZ(str,i + 1,xi)
                  "set t and p and flash"
                  valid_flsh ← mc_setOp(str,t,p)
                  "gas density from PPP"
                  ρ ← mc_StrGD(str)
                  (ρ valid_x valid_flsh)
```

$$(\rho \ valid_x \ valid_flsh) := GD\left(\text{stream}, \text{comp}, \frac{\text{Temp}}{\text{K}}, \frac{\text{Pressure1}}{\text{Pa}}\right)$$

$$\rho_{mix_1} := \rho \cdot \frac{\text{kg}}{\text{m}^3} = 10.941 \frac{\text{kg}}{\text{m}^3}$$

$$\text{valid}_x = \begin{pmatrix} 1 \\ 1 \\ 1 \end{pmatrix} \quad \text{valid}_\text{flsh} = 1 \quad \text{These variables should be 1 if there were no errors with PPP. They can be used to aid in debugging.}$$

$$(\rho \text{ valid_x } \text{ valid_flsh }) := \text{GD}\left(\text{stream}, \text{comp}, \frac{\text{Temp}}{\text{K}}, \frac{\text{Pressure2}}{\text{Pa}}\right)$$

$$\rho_{\text{mix_2}} := \rho \cdot \frac{\text{kg}}{\text{m}^3} = 4.729 \frac{\text{kg}}{\text{m}^3}$$

$$(\rho \text{ valid_x } \text{ valid_flsh }) := \text{GD}\left(\text{stream}, \text{comp}_{\text{atm}}, \frac{\text{Temp}_{\text{atm}}}{\text{K}}, \frac{\text{P}_{\text{atm}}}{\text{Pa}}\right)$$

$$\rho_{\text{mix_atm}} := \rho \cdot \frac{\text{kg}}{\text{m}^3} = 1.178 \frac{\text{kg}}{\text{m}^3}$$

size the receiver

$$\text{Vol}_{\text{drum}} := \frac{\text{time} \cdot \text{flow req} \cdot \rho_{\text{mix_atm}}}{\rho_{\text{mix_1}} - \rho_{\text{mix_2}}} = 5.155 \cdot \text{m}^3 \quad \text{The result compares well with the } 5.162 \text{ m}^3 \text{ obtained by Oscar Delgado.}$$

mc_ASave("") = 0

saved test2 archive