

## Piping-System Solutions Using Mathcad

### NOMENCLATURE

C equivalent lengths for minor loss coefficient

D pipe diameter

f Darcy friction factor

$f_T$  fully-rough friction factor

$g = 32.174 \frac{ft}{s^2}$  acceleration of gravity

$g_c$  conversion factor (English Engineering units),  $g_c := 32.174 \frac{ft \cdot lbm}{lbf \cdot sec^2} = 1$  (32.174 ft-lbm/lbf-sec<sup>2</sup>)

$h_d$  head change due to a pump, turbine, or other active device

K minor loss coefficient expressed as a number

L pipe length

N number of pipes, connection matrix

P pressure

Q flow rate

Re Reynolds number,  $VD/\nu$

V velocity

$W_s$  pump increase in head

o elevation

$\gamma$  specific weight,  $\gamma := \rho \cdot g$

$\epsilon$  absolute roughness of pipe,  $\epsilon := 0.045 \text{ mm}$ , steel pipe

$\mu$  viscosity,  $\mu_w := 0.01 \text{ poise} = 0.000672 \frac{lbm}{ft \cdot sec}$ , water at 20 deg centigrade

$\nu$  kinematic viscosity,  $\frac{\mu}{\rho}$ ,  $\nu := \frac{\mu_w}{\rho} = (1.077 \cdot 10^{-5}) \frac{ft^2}{s}$

$\rho$  density,  $\rho \equiv 62.4 \frac{lbm}{ft^3}$

### Subscripts

a upstream location

b downstream location

elbow elbow

ent entrance

exp expansion

gv gate valve

l arbitrary pipe in a pipe network

i counter

1 pipe 1

2 pipe 2

3 pipe 3

no matter how complex the piping system, the basis of all analysis and design calculations for piping systems is the energy-equation applied over a segment of a pipe. Consider, for example, a portion of a series-piping segment as illustrated schematically in Figure 1. If the flow is from "a" to "b," then the energy equation becomes

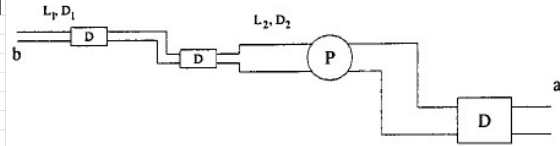


Figure 1 General piping system schematic.

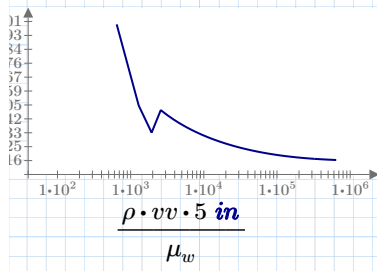
$$\frac{P_a}{\gamma} + \frac{V_a^2}{2 \cdot g} + z_a = \frac{P_b}{\gamma} + \frac{V_b^2}{2 \cdot g} + z_b + \sum_{i=1}^N \frac{8 \cdot Q^2}{\pi^2 \cdot g \cdot D_i^4} \cdot \left( f_i \cdot \frac{L_i}{D_i} + K_i + C_i \cdot f_{T_i} \right) - W_s \cdot \frac{g_c}{g} \quad (1)$$

It's instructive here to investigate the unit balance of this equation. Ascribe values with units:

Approximately water

$$\begin{aligned} \begin{bmatrix} P_a \\ P_b \end{bmatrix} &:= \begin{bmatrix} 15 \\ 10 \end{bmatrix} \cdot \text{psi} & \begin{bmatrix} V_a \\ V_b \end{bmatrix} &:= \begin{bmatrix} 10 \\ 15 \end{bmatrix} \cdot \frac{\text{ft}}{\text{sec}} \\ D &:= \begin{bmatrix} 3 \\ 3 \\ 1 \end{bmatrix} \cdot \text{in} & Q &:= 50 \text{ gpm} & L &:= \begin{bmatrix} 10 \\ 5 \\ 20 \end{bmatrix} \cdot \text{ft} & \begin{bmatrix} z_a \\ z_b \end{bmatrix} &:= \begin{bmatrix} 2 \\ 1 \end{bmatrix} \cdot \text{ft} & \text{ORIGIN} &:= 1 \\ i &:= 1 \dots 3 & K_i &:= 1 & C_i &:= 0.5 & f &= \frac{0.3086}{\log \left[ \frac{6.9}{Re} + \left( \frac{\epsilon}{3.7D} \right)^{1.11} \right]^2} & \text{For laminar flow, } f &= 64/Re. \end{aligned}$$

$$f(V, D) := \text{if} \left( \frac{\rho \cdot V \cdot D}{\mu_w} < 2100, \frac{64 \cdot \mu_w}{\rho \cdot V \cdot D}, \frac{0.3086}{\log \left( \frac{6.9 \cdot \mu_w}{\rho \cdot V \cdot D} + \left( \frac{\epsilon}{3.7 \cdot D} \right)^{1.11} \right)^2} \right) \quad vv := 1 \frac{\text{ft}}{\text{min}}, 2 \frac{\text{ft}}{\text{min}} \dots 1000 \frac{\text{ft}}{\text{min}}$$



$$f_T(D) := \frac{0.3086}{\log \left( \left( \frac{\epsilon}{3.7 \cdot D} \right)^{1.11} \right)^2} \quad \begin{aligned} f(V_a, D_1) &= 0.019 \\ f_T(D_1) &= 0.017 \end{aligned}$$

$$\begin{bmatrix} P_a \\ P_b \end{bmatrix} = \begin{bmatrix} 34.615 \\ 23.077 \end{bmatrix} \text{ft} \quad \begin{bmatrix} V_a^2 \\ V_b^2 \end{bmatrix} = \begin{bmatrix} 1.554 \\ 3.497 \end{bmatrix} \text{ft} \quad \begin{bmatrix} z_a \\ z_b \end{bmatrix} = \begin{bmatrix} 2 \\ 1 \end{bmatrix} \text{ft} \quad \sum_{i=1}^3 \frac{8 \cdot Q^2}{\pi^2 \cdot g \cdot D_i^4} \cdot \left( f(V_a, D_i) \cdot \frac{L_i}{D_i} + K_i + C_i \cdot f_T(D_i) \right) = 45.361 \text{ft}$$

The paper assumed:  $P_a = P_b, V_a = 0,$  and  $\frac{V_b^2}{2g} = \frac{8 \cdot Q^2}{\pi^2 g D_3^4}$

Then:

$$\begin{aligned} W_s \frac{g_c}{g} &= z_b - z_a + \frac{8 \cdot Q^2}{\pi^2 g D_1^4} \left[ 0.5 + 60f_{T1} + f_1 \frac{L_1}{D_1} \right] \\ &+ \frac{8 \cdot Q^2}{\pi^2 g D_2^4} \left[ 9 + f_2 \frac{L_2}{D_2} \right] \\ &+ \frac{8 \cdot Q^2}{\pi^2 g D_3^4} \left[ 1.0 + 55f_{T3} + f_3 \frac{L_3}{D_3} \right] \end{aligned}$$

Then for unit balance:

$$W_s := \frac{g}{g_c} \cdot z_a = 64.348 \frac{\text{ft}^2}{\text{sec}^2}$$

But  $W_s$  is pump increase in head

Start again

$$\frac{P_a}{\gamma} + \frac{V_a^2}{2 \cdot g} + z_a = \frac{P_b}{\gamma} + \frac{V_b^2}{2 \cdot g} + z_b + \sum_{i=1}^N \frac{8 \cdot Q^2}{\pi^2 \cdot g \cdot D_i^4} \cdot \left( f_i \cdot \frac{L_i}{D_i} + K_i + C_i \cdot f_{T_i} \right) - W_s \cdot \frac{g_c}{g} \quad (1)$$

$\gamma = \rho \cdot g$  multiply through by  $\gamma$

$$P_a + \frac{\rho \cdot V_a^2}{2} + z_a \cdot \rho \cdot g = P_b + \frac{\rho \cdot V_b^2}{2} + z_b \cdot \rho \cdot g + \sum_{i=1}^N \frac{8 \cdot \rho \cdot Q^2}{\pi^2 \cdot D_i^4} \cdot \left( f_i \cdot \frac{L_i}{D_i} + K_i + C_i \cdot f_{T_i} \right) - W_s \cdot \rho$$

$$P_a = 15 \text{ psi} \quad \frac{\rho \cdot V_a^2}{2} = 0.673 \text{ psi} \quad z_a \cdot \rho \cdot g = 0.867 \text{ psi} \quad \sum_{i=1}^3 \frac{8 \cdot \rho \cdot Q^2}{\pi^2 \cdot D_i^4} \cdot \left( f(V_a, D_i) \cdot \frac{L_i}{D_i} + K_i + C_i \cdot f_T(D_i) \right) = 19.657 \text{ psi}$$

To balance units, equation (1) should be:

$$\frac{P_a}{\gamma} + \frac{V_a^2}{2 \cdot g} + z_a = \frac{P_b}{\gamma} + \frac{V_b^2}{2 \cdot g} + z_b + \sum_{i=1}^N \frac{8 \cdot Q^2}{\pi^2 \cdot g \cdot D_i^4} \cdot \left( f_i \cdot \frac{L_i}{D_i} + K_i + C_i \cdot f_{T_i} \right) - W_s \quad (1)$$

Then the first effort,

$$W_s := z_a = 2 \text{ ft}$$

And the second effort,

$$W_s \cdot \gamma = 0.867 \text{ psi}$$

### Conclusions:

1. We really don't need the "gravitational constant,"  $g_c = 1$  since it doesn't supply anything.
2. The useable form (for Mathcad) of equation (1) is the red form above, which has balanced units.