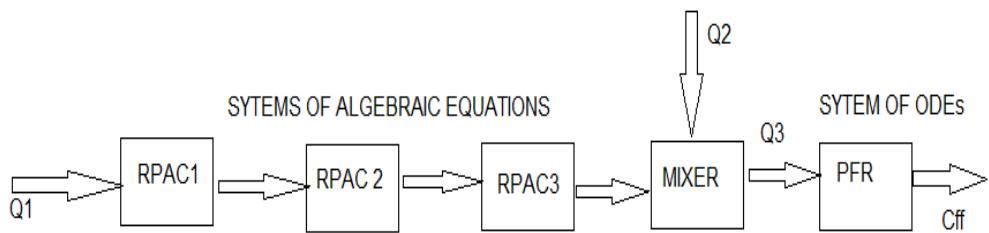


So my constraint in here its Q1 which can vary from 20 to 200

I had to find what value of Q1 in that interval gives the higher possible value of Cff at the end of this problem (**concentrations of F at the final reactor**)

I have 3 RPACs (**systems of algebraic equations like example 2**), values found in one are used as initial values in the next one. the flow coming out of the third RPAC mix with a stream in a mixer resulting in the incoming conditions for the Final reactor (**system of diff equation like example 3**).

Look at the diagram in the right for better understanding



What happens between RPACs it is not important neither what happens in the mixer, but what's coming out of the PFR (**differential equation system**),

Changing Q1 results in an augmentation of Q3 since $Q3 = Q1 + Q2$ (fixed)

How did I do it? I didn't know how to make it using Mathcad's function. So I proved values from 20 to 200, starting from 20 and increasing it by 5 until 200. I didn't have a good time :/.

Well I found the higher value of Cff by fixing $Q1 = 35$ ($Cff = 1.93$)

How would you maximize the value of Cff at the final reactor (system of ODEs) by changing Q1 (in the beginning of the systems of algebraic equations)?

Conditions initiales

$Ca_0 := 8$	$k1 := 0.01$	Varying this variable subject to:	Constraint:
$Cb_0 := 8$	$k2 := 0.005$	$Q1 := 115$	$20 \leq Q1 \leq 200$
$Cc_0 := 0$	$k3 := 0.02$		
$Cd_0 := 35$	$k4 := 0.001$		

Premier RPAC

Guess

$$Ca_1 := 5 \quad Cb_1 := 5 \quad Cc_1 := 3 \quad Cd_1 := 3 \quad Vr_1 := 50$$

Given

Bilans de matière

$$A: \quad Ca_0 = Ca_1 + k_1 \cdot Ca_1 \cdot Cb_1 \cdot \frac{Vr_1}{Q_1}$$

$$B: \quad Cb_0 = Cb_1 - 0.5 \cdot k_2 \cdot Cc_1 \cdot \frac{Vr_1}{Q_1} + k_1 \cdot Ca_1 \cdot Cb_1 \cdot \frac{Vr_1}{Q_1}$$

$$C: \quad Cc_0 = Cc_1 - k_1 \cdot Ca_1 \cdot Cb_1 \cdot \frac{Vr_1}{Q_1} + k_2 \cdot Cc_1 \cdot \frac{Vr_1}{Q_1}$$

$$D: \quad Cd_0 = Cd_1 - k_2 \cdot Cc_1 \cdot \frac{Vr_1}{Q_1}$$

$$\begin{pmatrix} Ca_1 \\ Cb_1 \\ Cc_1 \\ Cd_1 \end{pmatrix} := \text{Find}(Ca_1, Cb_1, Cc_1, Cd_1)$$

Les Concentration à la sortie

$$Ca_1 = 7.74$$

$$Cb_1 = 7.74$$

$$Cc_1 = 0.26$$

$$Cd_1 = 35.001$$

Deuxième RPAC

Guess

$$Ca_2 := 1 \quad Cb_2 := 1 \quad Cc_2 := 1 \quad Cd_2 := 1 \quad Vr_2 := 100$$

Given

Bilans de matières

$$A: \quad Ca_1 = Ca_2 + k_1 \cdot Ca_2 \cdot Cb_2 \cdot \frac{Vr_2}{Q_1}$$

$$B: \quad Cb_1 = Cb_2 - 0.5 \cdot k_2 \cdot Cc_2 \cdot \frac{Vr_2}{Q_1} + k_1 \cdot Ca_2 \cdot Cb_2 \cdot \frac{Vr_2}{Q_1}$$

$$C: \quad Cc_1 = Cc_2 - k_1 \cdot Ca_2 \cdot Cb_2 \cdot \frac{Vr_2}{Q_1} + k_2 \cdot Cc_2 \cdot \frac{Vr_2}{Q_1}$$

$$D: \quad Cd_1 = Cd_2 - k_2 \cdot Cc_2 \cdot \frac{Vr_2}{Q_1}$$

$$\begin{pmatrix} Ca_2 \\ Cb_2 \\ Cc_2 \\ Cd_2 \end{pmatrix} := \text{Find}(Ca_2, Cb_2, Cc_2, Cd_2)$$

Les Concentration a la sortie

Ca2 = 7.279

Cb2 = 7.281

Cc2 = 0.718

Cd2 = 35.004

Troisieme RPAC

Guess

$$Ca_3 := 0 \quad Cb_3 := 0 \quad Cc_3 := 0 \quad Cd_3 := 0 \quad Vr_3 := 500$$

Given

Bilans de matieres

$$A: \quad Ca_2 = Ca_3 + k1 \cdot Ca_3 \cdot Cb_3 \cdot \frac{Vr_3}{Q_1}$$

$$B: \quad Cb_2 = Cb_3 - 0.5 \cdot k2 \cdot Cc_3 \cdot \frac{Vr_3}{Q_1} + k1 \cdot Ca_3 \cdot Cb_3 \cdot \frac{Vr_3}{Q_1}$$

$$C: \quad Cc_2 = Cc_3 - k1 \cdot Ca_3 \cdot Cb_3 \cdot \frac{Vr_3}{Q_1} + k2 \cdot Cc_3 \cdot \frac{Vr_3}{Q_1}$$

$$D: \quad Cd_2 = Cd_3 - k2 \cdot Cc_3 \cdot \frac{Vr_3}{Q_1}$$

$$\begin{pmatrix} Ca_3 \\ Cb_3 \\ Cc_3 \\ Cd_3 \end{pmatrix} := \text{Find}(Ca_3, Cb_3, Cc_3, Cd_3)$$

Les Concentration a la sortie

Ca3 = 5.807

Cb3 = 5.832

Cc3 = 2.143

Cd3 = 35.05

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courrant d'entre

$$Q1 = 115$$

$$Q2 := 30$$

Courrant sortant des RPAC

$$Ca3 = 5.807$$

$$Cb2 = 7.281$$

$$Cc3 = 2.143$$

$$Cd3 = 35.05$$

Courrant de produit E

$$Ce := 10$$

Bilan de matière

Q3 DEPENDS OF Q1, Q2 IS FIXED

$$Q3 := Q1 + Q2$$

$$Ca3 \cdot Q1 = Ca4 \cdot Q3$$

$$Cb3 \cdot Q1 = Cb4 \cdot Q3$$

$$Cc3 \cdot Q1 = Cc4 \cdot Q3$$

$$Cd3 \cdot Q1 = Cd4 \cdot Q3$$

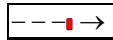
$$Ce \cdot Q2 = Ce4 \cdot Q3$$

$$Ca4 := \frac{Ca3 \cdot Q1}{Q3}$$

$$Cd4 := \frac{Cd3 \cdot Q1}{Q3}$$

$$Cb4 := \frac{Cb3 \cdot Q1}{Q3}$$

$$Ce4 := \frac{Ce \cdot Q2}{Q3}$$



$$Cc4 := \frac{Cc3 \cdot Q1}{Q3}$$

Courrant de sortie

$$Q3 = 145$$

$$Ca4 = 4.605 \quad Cd4 = 27.799$$

$$Cb4 = 4.625 \quad Ce4 = 2.069$$

$$Cc4 = 1.7$$

Reacteur Tubulaire

Concentrations d'entre

$$Ca4 = 4.605$$

$$Ce4 = 2.069$$

$$Cb4 = 4.625$$

$$Cf4 := 0$$

$$Cc4 = 1.7$$

$$Cg4 := 0$$

$$Cd4 = 27.799$$

Given

Bilans de matière

$$A: \frac{d}{d\tau} Ca(\tau) = -k1 \cdot Ca(\tau) \cdot Cb(\tau)$$

B: $\frac{d}{d\tau} C_b(\tau) = -k_1 \cdot C_a(\tau) \cdot C_b(\tau) + 0.5 \cdot k_2 \cdot C_c(\tau)$

C: $\frac{d}{d\tau} C_c(\tau) = k_1 \cdot C_a(\tau) \cdot C_b(\tau) - k_2 \cdot C_c(\tau) - k_3 \cdot C_c(\tau) \cdot C_e(\tau)$

D: $\frac{d}{d\tau} C_d(\tau) = k_2 \cdot C_c(\tau) + k_3 \cdot C_c(\tau) \cdot C_e(\tau) - k_4 \cdot C_f(\tau) \cdot (C_b(\tau) \cdot C_d(\tau))^{0.5}$

E: $\frac{d}{d\tau} C_e(\tau) = -k_3 \cdot C_c(\tau) \cdot C_e(\tau)$

F: $\frac{d}{d\tau} C_g(\tau) = k_4 \cdot C_f(\tau) \cdot (C_b(\tau) \cdot C_d(\tau))^{0.5}$

G: $\frac{d}{d\tau} C_f(\tau) = k_3 \cdot C_c(\tau) \cdot C_e(\tau) - k_4 \cdot C_f(\tau) \cdot (C_b(\tau) \cdot C_d(\tau))^{0.5}$

$$C_a(0) = Ca4 \quad C_b(0) = Cb4 \quad C_c(0) = Cc4 \quad C_d(0) = Cd4$$

$$C_e(0) = Ce4 \quad C_f(0) = Cf4 \quad C_g(0) = Cg4$$

$$\begin{pmatrix} Caf \\ Cbf \\ Ccf \\ Cdf \\ Cef \\ Cff \\ Cgf \end{pmatrix} := \text{Odesolve} \left[\begin{pmatrix} Ca \\ Cb \\ Cc \\ Cd \\ Ce \\ Cf \\ Cg \end{pmatrix}, \tau, 300 \right]$$

Reacteur V= 2000

Concentrations à la sortie

$$Vr1 := 2000 \quad \tau1 := \frac{Vr1}{Q3}$$

As you can see the variable $\tau1$ (TAU) only depends on Q3 since Vr1 is fixed. and Q3 depends on Q1.

$$\tau1 = 13.793$$

$$Caf(\tau1) = 2.798$$

$$Cbf(\tau1) = 2.893$$

$$Ccf(\tau1) = 2.42$$

$$Cdf(\tau1) = 28.823$$

$$Cef(\tau1) = 1.132$$

$$Cff(\tau_1) = 0.874$$

I WANT TO FIND THE MAXIMUM VALUE OF Cff CHANGING Q1

$$Cgf(\tau_1) = 0.063$$

